

Energy Production from Thermal Gasification of Selected Solid Wastes from Kiambu County, Kenya

Mugo Ephantus¹, Kinyua Robert², Yasuyuki Nemoto³, Njogu Paul⁴

^{1, 2, 4}Institute of Energy and Environmental Technology, Jomo Kenyatta University of Agriculture and Technology, P. O. Box 62000-00200, NAIROBI, KENYA.

³Division of Renewable Energy and Environment, Ashikaga Institute of Technology, Japan

Abstract: Increased population growth resources competition and the diminishing of conventional energy sources calls for development of innovative technologies for power generation. Thermal gasification is a promising technology for conversion of carbonaceous waste into energy resources such as synthesis/producer gas (methane, carbon monoxide (CO), hydrogen (H) and carbon dioxide (CO₂) and other gases). The study assessed the potential for conversion of rice husks, maize cobs and sawdust to energy resources by thermal gasification using a locally assembled gasifier. Rice husks, maize cobs and sawdust samples were collected and dried to a moisture content of <8%. The process parameters that were controlled included temperature, pressure, process time and air injection. The resultant gas was upgraded by passing it through a series of wood shavings filters before collecting it for analysis. Portions of 1cm³ syngas samples were sampled and injected into a gas chromatograph with thermal conductivity detector (GC-TCD) to determine the concentration of CO₂, CO, CH₄, H₂, N₂, and O₂. Results show that 25Kg of rice husks, produced 580±4.2 m³ of syngas, while sawdust and maize cobs produced 480±2.8 m³ and 420±3.1 m³ respectively. Syngas derived from rice husk contained 9.81±0.99% CH₄, 28.55±0.99% CO, 12.59±0.99% CO₂, 7.44±0.99% N₂, 8.34±0.99% O₂ and 34.06±1% H₂ while that from sawdust contained 12.06±1.13% CH₄, 34.34±1.13% CO, 8.24±1.1% CO₂, 5.11±1.1% N₂, 5.96±1.13% O₂ and 34.4±1.1% H₂ respectively. The calorific value of syngas derived from sawdust was approximately 16 MJ/m³. Rice husks and maize cobs produced 13 MJ/m³ and 12 MJ/m³ respectively. The high content of CH₄ and CO in sawdust contributes to its higher calorific value than rice husk. This gas is therefore sufficient to directly drive a 10-kWe AC synchronous generator at a speed of 1,800 rpm producing 220 volt current, which can supply a total of 16 pieces of 50-watt bulbs, can be energized by the plant for 8 to 10 hours continuous operation. The results indicate that there is potential of energy production from carbonaceous wastes. Independent power producers can adopt this waste to energy (WtE) conversion technology.

Keywords: Solid wastes, gasification, WtE, rice husks, saw dust, maize cobs, syngas

1. Introduction

Gasification or controlled partial oxidation of a carbonaceous material, and it is achieved by supplying less oxygen than the stoichiometric requirement for complete combustion. Air (or oxygen in some applications) is used as a gasification agent, and the air factor is generally 20% - 40% of the amount of air needed for the combustion (Daniela *et al.*, 2002). A central process between combustion (thermal decomposition with excess oxygen) and pyrolysis (thermal decomposition in the absence of oxygen), it proceeds at temperatures ranging between 600°C and 800°C. Depending upon the process type and operating conditions, low- or medium-value producer gas (which is a combination of combustible and non-combustible gases) is created (Doherty *et al.*, 2009; Jaouaruek *et al.*, 2011). The main feature of this technology is its ability to produce a reliable, high-quality synthesis gas (syngas) product that can be used for energy production. The primary product of this gaseous mixture is carbon monoxide and hydrogen, with minor percentages of gaseous hydrocarbons also formed. The thermo chemical conversion changes the chemical structure of the biomass by means of high temperature. The gasification agent allows the feedstock to be quickly converted into gas by means of different heterogeneous reactions (Kathirvale *et al.*, 2004; Narvaez *et al.*, 2004; Singh *et al.*, 2011). The combustible gas contains CO₂, CO, H₂, CH₄, H₂O, trace amounts of higher hydrocarbons, inert gases present in the gasification agent, various contaminants

such as small char particles, ash and tars (Themelis *et al.*, 2003).

2. Materials and Methods

2.1 Area of Study

This study was carried out in Thika Municipality of Kiambu County. The study area lies between latitudes 3°53' and 1°45' south of Equator and longitudes 36°35' and 37°25' east (Robinson *et al.*, 2005).

2.2 Sample Collection

Rice husks, maize cobs and saw dust samples were collected in pre cleaned polyethylene bags, screened to remove large particles and sun dried to a constant weight before storage.

2.3 Sample Treatment

Rice husks, maize cobs and saw dust samples were dried by spreading them outside sunlight to reduce the moisture content. Samples of this waste were taken and tested to monitor the moisture levels before gasification.

2.4 Data Collection

Portions of 25 Kgs were fed into the gasifier and process parameters set.

2.4.1 Thermal gasification of selected waste

A gasifier with 40 cm internal diameter and a height of 200cm reactor equipped with an electric air blower to provide the air needed in gasifying the feedstock was used. These samples were manually fed to the reactor from the top. On the other hand, char is removed from beneath the gasifier at the char box. The gas coming out of the reactor is conditioned by allowing it to pass through the gas-cleaning devices which consisted of wet scrubbers, tar condenser cyclone, and a series of two wood shavings packed filters. Fig. 1 shows the engineering drawing of an updraft gasifier used to undertake this experiment.

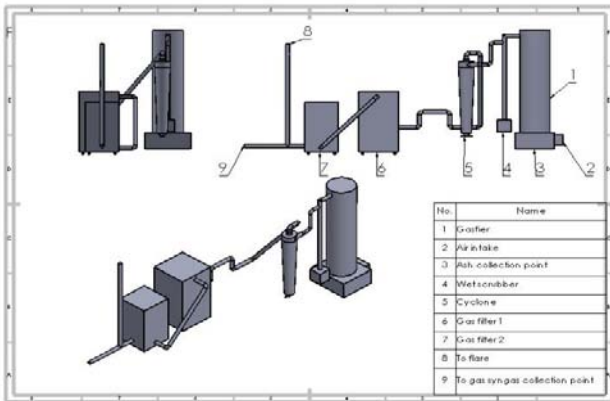


Figure 1: Engineering drawing of an updraft gasifier used to undertake this experiment

2.4.2 Compositional analysis of syngas

Syngas was analyzed as described by the American Standard Test method ASTM D2504-88(1998). Gas chromatograph with thermal conductivity detector (GC-TDC) model Shimadzu GC-8A and gas chromatography flame ionization detector (GC-FID) model Shimadzu GC-9A were used for the analysis. An isocratic mode was used since a constant temperature was maintained throughout the operation.

Portions of 1 ml samples were injected into a gas chromatograph (GC-TCD) and the CO₂, CO, CH₄, H₂, N₂, and O₂ concentrations were determined using a (TCD). The equipment were calibrated using gas standards and the gases identified based on the retention time and the concentrations calculated from the peak areas. Analysis parameters used are as shown in the table 2.1.

Table 2.1: Operational conditions and analysis parameters

Column Width 6	Slope 50
Drift 0	MIN. AREA 100
T.DBL 0	STOP. Time 6
Attenuation factor 4	Speed 10
Method 41	Format 0

Test was carried out in JKUAT food science laboratories.

3. Results and Discussion

3.1 Gasification of Rice husks, maize cobs and saw dust

The gasification experiment was operated at specified parameters and it yielded the results shown in Table 3.1.

Table 3.1: Operation process parameters for gasification

Type of feedstock - Rice husks	Measured value		
	Rice husks	Sawdust	Maize cobs
Total operation time (min)	150	180	120
Moisture content(% wet basis)	7	7.8	7.5
Initial weight of feed (kg)	25	25	25
Feed in air (m ³ /min)	8.2	8.2	8.2
Average reduction zone temperature (at the bottom) (°C)	510±2.3	410±2.1	420±3.1
Average drying zone temperature (at the top) (°C)	222±1.9	222±1.7	220±2.1
Estimated gas yield (m ³)	580±4.2	480±2.8	420±3.1
Average calorific value of syngas (MJ/Nm ³)	13.18 ±0.12	16.17±0.23	12.1±0.18

It took the gasifier between two and three hours to decompose the same amount of various feedstock used, with an average of 8.2 m³/min of feed in air.

3.2 Syngas composition data

The syngas generated was analyzed to establish its composition. Concentration versus peak area values was obtained for each standard gas and the sample concentrations were obtained from the appropriate calibration curves. For compound identification, standard gases were used. Fig.2. Chromatograms of the gas analysis, using Gas chromatograph thermal conductivity detector (GC-TDC) for each gas sample were used

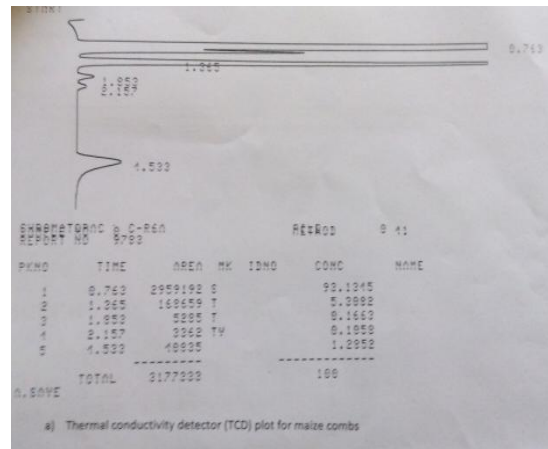
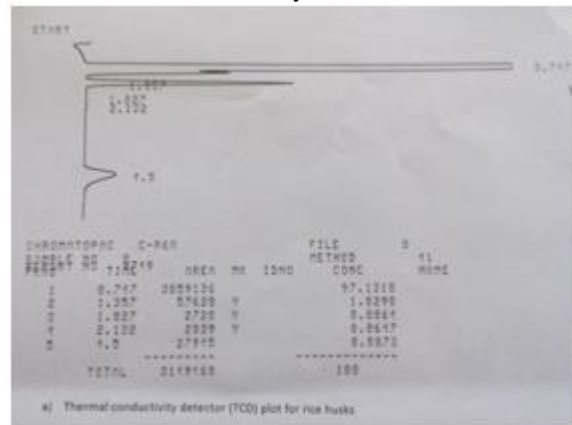


Figure 2: Shows some of the Chromatograms for this analysis



The composition of syngas is presented in Table 2.

Table 2: Syngas composition data of selected waste

Parameters measured	Syngas from rice husk Average conc (ppb)	Abundance %	Syngas from sawdust Average conc (ppb)	Abundance %	Syngas from maize comb Average conc (ppb)	Abundance %
CH ₄	9.18±0.31	9.81±0.99	13.60±1.76	12.06±1.13	24.74±2.70	22.02±1.10
CO	28.84±0.25	28.55±0.99	38.72±3.06	34.34±1.13	27.90±1.64	24.83±1.12
CO ₂	12.61±3.55	12.59±0.99	9.29±4.53	8.24±1.10	9.99±1.52	8.89±1.12
N ₂	7.51±0.15	7.44±0.99	5.76±0.76	5.11±1.10	7.44±0.11	6.62±1.10
O ₂	8.22±0.25	8.34±0.99	6.72±0.74	5.96±1.13	11.97±0.58	10.65±1.12
H ₂	34.4±0.12	34.06±0.99	38.79	34.40±1.10	30.32±0.74	30.32±1.12

3.3 Estimation of energy derived from gasification of MSW

While using saw dust the average volume of gas generated was 480m³. The calorific value of this of the syngas is 16.17 MJ/m³. This is equivalent to 4527.6 MJ. While using rice husks the average volume of gas generated was 580m³. The calorific value of this of the syngas is 13.18 MJ/m³. This is equivalent to 7644.4 MJ. While using maize cobs the average volume of gas generated was 420m³. The calorific value of this of the syngas is 12.1 MJ/m³. This is equivalent to 5082.0 MJ

Assuming 50% thermal efficiency of the gas driven engine, then output energy of the engine is:

$$4527.6MJ \times 50\% = 2263.8 MJ$$

$$7644.4MJ \times 50\% = 3822.2 MJ$$

$$5082.0MJ \times 50\% = 2541.0MJ$$

This is the mechanical input fed to a generator. Assuming the generator and the speed governor operate at 35% efficiency and using the relationship of 1 kWh of electricity output = 3.6 MJ then,

$$\frac{2263 \times 35\%}{3.6} = 220.1Kwh - \text{for saw dust}$$

$$\frac{3822.2 \times 35\%}{3.6} = 371.6 kwh - \text{from rice husk}$$

$$\frac{2541.0 \times 35\%}{3.6} = 247.04 Kwh - \text{from maize cob}$$

This gas is therefore sufficient to directly drive a 10-kWe AC synchronous generator at a speed of 1,800 rpm producing 220 volt current, which can supply a total of 16 pieces of 50-watt bulbs, can be energized by the plant for 8 to 10 hours continuous operation. Therefore the result shows that if this waste at the dumpsite was gasified it contains a lot of energy potential, whereby if a gasifier of higher efficiency is used there exists potential of converting this waste to useful energy resource.

3.4 Syngas as a fuel for modified diesel engine.

The gas was fueled to drive an engine. The engine ran at variable speed of between a minimum of 1852 to maximum of 3856 rpm. Shaft speed of the engine was measured using a digital tachometer as shown in figure 3. The engine is entirely fueled by the gas generated, except at the start-up and at the end of the operation. The output of this engine shaft is coupled to generator to produce output electrical power.



Figure 3: measuring the shaft speed of a gas driven engine using a digital tachometer

4. Conclusion

With the increasing industrialization and rapid population growth non renewable fuels are rapidly getting consumed, which may lead to risk of energy shortage in the future, but a definite solution to it is the use of renewable source. Conversion of waste to energy through gasification can be a good solution. Kenya being an agricultural country, there is ready availability of agricultural residues such as rice husk and maize cobs whereby adopting these gasifiers who produce a change in the energy scenario of the country.

5. Acknowledgement

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