

Technological Revolution in Drying of Fruit and Vegetables

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Abstract: Historical evolution of different drying methods for drying fruit and vegetables was evolved gradually with time. Nowadays, every form of fruit and vegetables slices, chunks, paste, puree, solution can be dried using different available dryers. Recent research on drying methods focuses on the advancement in of energy consumption, product recovery and preservation of nutrients. Different combination dryers are also used as advancement for a particular dryer. Technological advancements in drying methods were triggered by the shortcomings of the existing one. This revolution clearly indicates that drying not only reduces moisture content to a safe storage level but also provides different edible forms.

Keywords: History, Drying methods, Fruits and vegetables

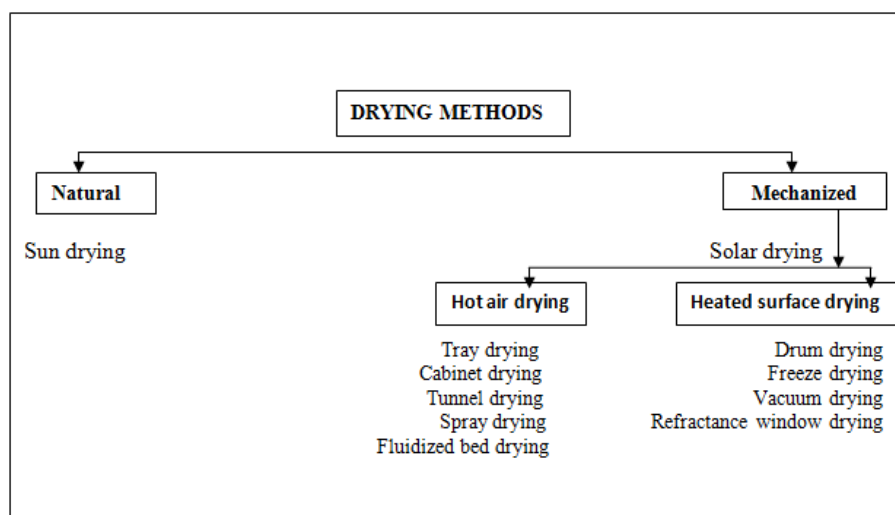
1. Introduction

Keeping the product fresh is the best way to maintain its nutritional value, but most storage techniques require low temperatures, which are difficult to maintain throughout the distribution chain. On the other hand, drying is a suitable alternative for post harvest management especially in countries like India where exist poorly established low temperature distribution and handling facilities. It is noted that over 20% of the world perishable crops are dried to increase shelf-life and promote food security. It is the oldest and most effective method of lowering water content in order to slow down food spoilage by micro-organisms.

Commonly three words are used to express the removal of water from a food product “drying” or “dehydration”, or “dewatering”. Vega- Mercado et al. (2001) explained that these words are used to differentiate the process according to the level of water removed (Mulet, 2011). “Drying” of food material occurs when water vapour is removed from its surface into the surrounding space, resulting in a relatively dried form of the material. In “dewatering”, liquid water is drained or squeezed out of the material. In “dehydration” evaporation of water takes place initially the surface water (external diffusion) then from interior

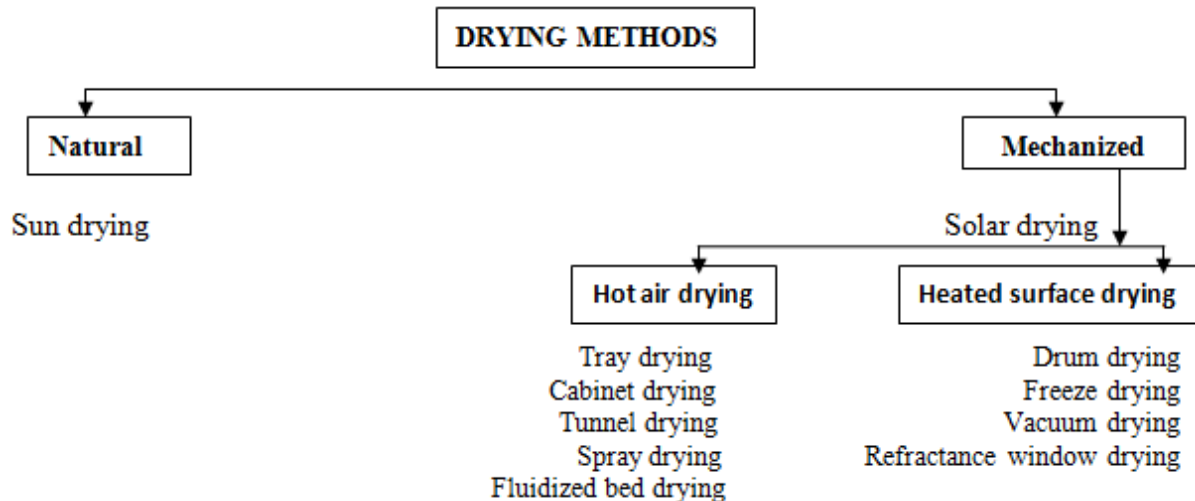
surface of raw material (internal diffusion). If the rate of external diffusion is far greater than internal diffusion it leads to over dehydration i.e ‘case hardening’. When the water concentration in the interior is too high its water vapour pressure will be too high. This causes cracking of the more tender tissues and thus the cracking of the surface with leaching of the soluble substances from the interior, affecting negatively the appearance and quality of the final product.

The use of artificial drying to preserve agricultural products has expanded widely, creating a need for more rapid drying techniques and methods that minimize the amount of energy used in these processes. Thus, innovative techniques to increase drying rates and enhance final product quality have gained considerable. Many of the drying technologies are the outcome of the ‘technological revolution’ of the pre- and post-war periods (1940-1950). Moreover, the space programme (1950-1990) also brought in its wake technologies that were soon to become a part of our food industry’s currency (Henry, 1997). It shift in focus of drying of agriculture produce has been observed that in past it was mainly to increase the shelf life but nowadays efforts have been made in developing high quality dried fruits and vegetables.



American Indians made dried mashed potatoes about 3500 BC ago. The earliest recorded mention of dried fruits can be found in Mesopotamian tablets dating to about 1700 B.C (Brothwell D et al. 1998). In 1780 AD, the first patent on vegetable drying was taken out in America. The vegetables were boiled in salt water, and kept for 20-30 hours. The quality was poor. In 1795 AD, in France, sliced vegetables were dried in air at 40°C, pressed, and sealed in foil. Recently, however, efforts have been made to develop high-quality dried fruits and vegetables (Sablani 2006). Drying process could be hastened and improved by

various mechanical techniques. For example, the Arabs learned early on that apricots could be preserved almost indefinitely by macerating them, boiling them, and then leaving them to dry on broad sheets (World of Microbiology and Immunology 2003). The search for new food product categories and improvements in existing technologies often trigger technological changes of a revolutionary or an evolutionary nature. In this revolution the technologies came in light as follows:



Other novel methods include: Osmodehydration, Microwave heating, and Infrared, Ohmic heating, Pulsed Electric Field (but all these are used as a part of hurdle technology i.e used as pretreatments to increase efficiency of conventional drying methods)

I. Natural Dryers

Sun drying is oldest method of preservation method for fruits and vegetables. The ancient Hindus and Chinese used to dry fruits & vegetables by the sun and wind around 5000 years ago In Pakistan Early Bronze Age (3,300 to 2,100 B.C.E.) raisins and dried figs are identified in an archaeobotany study (Milczarek, (2013).

II. Mechanized Dryers

After sun drying, in late 1700s French people used controlled air and temperature to dry fruits and vegetables introduction of air to increase drying efficiency was observed. According to Vega Mercado et.al. 2001 mechanized dehydration methods can be classified into four generations in order of their historical development.

- **First generation dryers** Cabinet and bed type dryer (such as kiln, tray, truck, rotary, conveyor and tunnel)
- **Second generation dryers**, spray drying, drum drying, fluidized bed drying,
- **Third generation dryers** freeze drying, high vacuum, osmodehydration drying
- **Fourth generation dryers**, flash microwave, infrared, combined method, refractance window, high electric field drying.

1. Solar Drying

At the end of 1800s and beginning of 1990s sun drying is replaces by artificial drying (Van Arsdel and Copley, 1963). WWI & WWII introduced improved dehydration for commercial operation. First record of drying vegetables mechanically appeared in 18th century (Van Arsdel and Copley, 1963) is considered as improved form of sun drying. It is a controlled efficient system which utilizes solar energy (Bala, 1997a & 1998, Zaman and Bala, 1989 and Muhlbauer, 1986). Solar driers can generate higher air temperatures and lower relative humidity (Brett et al., 1996b)

2. Tray Drying

It is simple in design and has capability to dry products at high volume. In 1795 fist hot air dehydrator was used to dry fruits like prunes, raisins, apricots etc. The key to the successful operation of the tray dryer is uniform airflow distribution over the trays (S. Misha et al. 2013). Colak and Hepbasli, 2007 developed model for green olives The first reported study on energy efficiency of dehydrators was conducted by (Cruess and Christie, 1921) when heated, forced-air dehydrators were introduced as a substitute for sundrying of prunes However, the greatest drawback of the tray dryer is uneven drying because of poor airflow distribution in the drying chamber. Implementing the proper design of a tray dryer system may eliminate or reduce non-uniformity of drying and increases dryer efficiency. Most of the dryer systems have been developed are using solar energy because the systems run at low operating cost.(Misha et.al., 2013).

Das et al., 2001 designed and developed a tray to remove the void space re-circulatory cabinet dryer using a central air distribution. Before loading of next batch previous was unloaded to uniform moisture distribution by hot air.

3. Cabinet Drying

These are simplest solar dryers of very low capacity and were mainly used to dry fruits and vegetables. (Mujumdar,) During 1870-1890 first steam heated radiator was used in New York. they are used for drying fruits (grapes, dates, apples), vegetables (onion, cabbage) and although the cost of the equipment is low, but its operating (labour) cost is high. Shawik Das et al. (2001) for potatoes chip, (Al-Juamily et al., 2007) for grapes, apricot and beans developed different models.

4. Tunnel Dryers

Tunnel dryers brought tremendous changes and advantages into food industry (Earle, 1992). These are considered as developments of the tray & cabinet dryer in which the trays on trolleys move through a insulated tunnel where the heat is applied and the vapors are removed (Brennan, 2006). It was introduced as heated forced air dryer as substitute of sun drying of prunes (Thompson et al., 1981. Ratti and Crapiste, 1992) proposed a receding front modeling convecting heat and mass transfer for different food products such as potato, apple and carrot. This method is often used to dry apricots, peaches, pears, apples, figs, dates, and so on in form of pieces, purees, liquids.

5. Drum Drying

Drum drying was started about 120 years ago i.e early 1900s and first drum drier was developed by, Just Hatmaker in 1902. Firstly double drum dryer with feed flowing into the nip was developed (Van't Land., 2012.) which was less suitable for viscous fluids hence in 1945 single drum with top feed was introduced to handle viscous products. Feed application in single drum was dipping, splashing, spraying and bottom feed roll. Feeding method is generally based on the viscosity of the feed. The drum drying parameters such as drying temperature, feed rate, rotation speed, feed concentration, and surrounding air condition are influential to the attributes of drum-dried food such as particle size, bulk density, moisture content, and solubility (Nastaj, 2000; Pua et al., 2010).

6. Spray Drying

The development of spray drying equipment and techniques evolved over a period of several decades from the 1870s through the early 1900s. The first mention of the application of this drying method comes from the year 1860, and the first patent concerning spray drying was registered in 1872, (US patent Percy, 1872). For improvement in drying and concentrating liquid substances by atomizing, (Cal and Solohub, 2009). In 1912, George Krauss developed the centrifugal spray drier and in 1913 Grey and Jensen developed a conical spray drier. The first spray dryers were manufactured in the

USA in 1933, (Phisut, 2012). Free flow powder of fruits and vegetables was made by spray drying in 1950 after that since late 1950s spray drying encapsulation has been used in the food industry. It was firstly used for the tomato juice dehydration (Kaufman, 1958), and Kraftco Corp was the first company in 1970 which manufactured spray dried tomato products. (Samuel Percy, 1972). The first known spray dryers used nozzle atomizers, with rotary atomizers introduced several decades later. The true boom in spray drying technology was driven by World War II. dried with additives (Mujumdar, 2004).

7. Fluidized Bed Dryers

It is a modification of belt trough dryer as it eliminates risk of soluble material migrating and uses heated air flow beneath the bed to lift the food particles & same time convey them outside. In food Fluidized Bed Drying came after 1960s. It is used extensively for the drying of wet particulate and granular materials that can be fluidized, and even slurries, pastes, and suspensions that can be fluidized in beds of inert solids (Law and Mujumdar, 2006.). This drying method is mainly used for vegetables like peas, green beans and carrots (Cohen et al. 1994), onion slices onion drying. Mujumdar has reported more than 30 variants of fluidized bed dryer and these are preferred over other drying system for particulate drying as very high heat and mass transfer can be achieved.

8. Freeze Drying

History goes back to the ancient Inca's, the Indian tribes of Peru in the South American mountain, who preserved their food stuff by freezing it in the mountains in winter time. At the same time the frozen water is removed through the low vapour pressure of the water (below 0.6 kPa pressure (the triple point of water) (Maharjan, 1995).) in the surrounding air at those high altitudes sun as early as 3500 B.C. Andean civilization (Indian tribes of Peru) first used this method to preserve potatoes (chuno). (Timothy, 1990) Before 1930s in second world war troops were supplied freeze dried orange juice and after 1960, it become commercialized (NHCL, 2002). In 1945, Flosdorf first used vacuum freeze drying for foods. Of course this process was rather slow, but during the drying process the quality of the food was maintained due to its frozen state. Research into freeze drying was undertaken in the UK in the early 1950s which led to the development of the accelerated freeze drying (AFD) method. In 1960, the first freeze-dried instant coffee was produced. Today in mechanical process food is first frozen (-20°C) and then a controlled amount of heat under vacuum is applied to promote sublimation during which ice is directly changed to vapor and subsequently condenses as ice on a refrigeration coil, typically held at -55°C (Claussen et al. 2007, Oetjen and Haseley, 2004; Barbosa-Cánovas and Vega-Mercado, 1996). Industrial application includes some exotic fruits and vegetables, soup ingredients, mushrooms, and orange juice, Mango pulp (Caparino et al. 2012), Onion Stalk (Kushwaha, 2012) passion fruit juice, coffee, pineapple, Barbados cherry, guava, guava pulp, papaya mushrooms, carrot, capsicum and strawberries (Marques et al., 2006)

9. Vacuum Drying

First patent for vacuum drying was registered in 1922 for wood drying system in Sweden. In early 20th century vacuum technology was used along with freeze drying for drying of various food products (Mujumdar, 1995). In vacuum there is no air therefore no partial pressure, so absolute pressure is termed as water vapour pressure. Pressure driven flow is the dominant transport in moisture migration in vacuum drying (Cenkowski et al., 2008). It is done below the pressure of 101 kPa but above 0.6 kPa, in which the heat transfer is usually done by conduction method. (Maharjan, 1995).. Under vacuum water boils at low temperature due to pressure, thus drying time is shortened by drying rate. Also the water circulation inside the product increase which results in high mass transfer.

10. Osmodehydration

In 1966, Pointing and co-workers pioneering the research on OD of foods (Pointing et al., 1966), and since after that a continuous stream of publication was appeared (Rastogi et al., 2002). By using of osmosis process 50% of original weight of fruit was reduced, after that it was subjected to freeze or vacuum dried. It was successfully applied on apples (Farkas and Lazar, 1969; Vial et al. (1991), papaya

and kiwi (Heng, 1990). It is the process of water removal by immersion of water containing cellular solids in a aqueous solution (Syrup and brine). The driving force for water removal is the chemical solution and the intracellular fluid. Due to complexity of food it is difficult to obtain perfect semi-permeable membrane as leaching out of food’s own solute can occur. The process is characterized by equilibrium and dynamic periods. In dynamic period the mass transfer rate is increased or decreased until equilibrium is reached i.e net mass transfer becomes zero. Removal of water is mainly by diffusion and capillary flow whereas uptake is only by diffusion (Rahman, 2006).

11. Refractance Window Drying

Refractance Window™ Technology is a novel drying system, developed by the owners of MCD Technologies, Inc. in Tacoma, Washington in 1989. It uses circulating water at atmospheric pressure as a means to carry thermal energy to material to be dehydrated. The products are spread on a transparent plastic conveyer belt and unused heat is recycled. Products on the moving belt dry in a few minutes, contrary to hot air tray or tunnel dryers which take several hours, or freeze dryers which dry overnight.

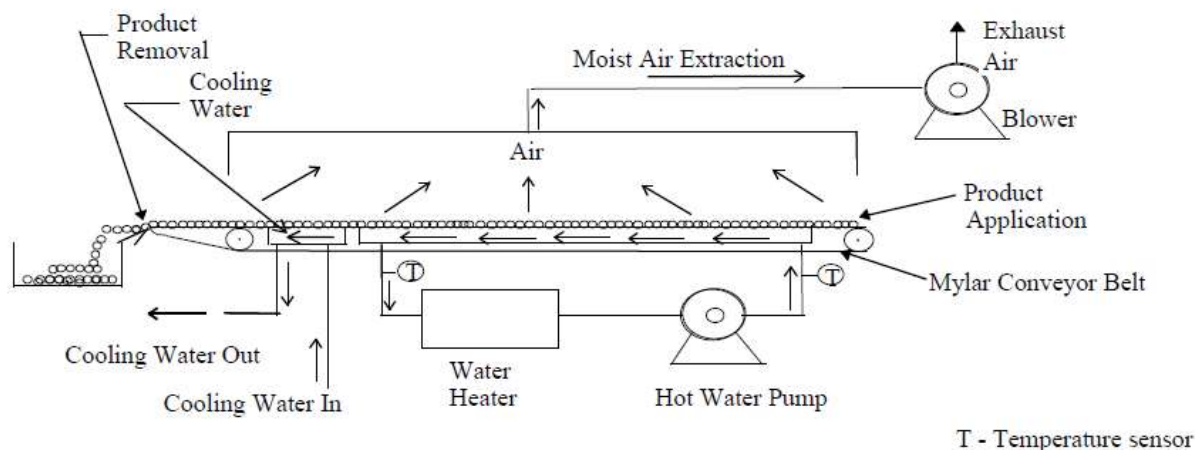


Figure 1: Schematic diagram of Refractance Window™ drying system

| S.No | Drying | Mode of operation | Type of Feed | Advantages | Disadvantages | Technological revolution |
|------|---------------|-------------------|---------------------|--|--|--|
| 1. | Sundrying | C | Whole, Slice chunks | Large capacity inexpensive | Long drying times Poor product quality (excessive browning and casehardening) unhygienic | Hybrid drying system with tray, osmotic dehydration system etc. |
| 2. | Solar drying | B | Whole, Slice chunks | Better product quality than sun drying Utilization of renewable energy i.e cost effective | Short drying time Hygienic Less capacity | Solar assisted drying such as tray, tunnel, vacuum, osmotic dehydration, greenhouse type |
| 3. | Cabinet dryer | B | Whole, Slice chunks | Simplest solar dryer | Thermal efficiency low | |

| | | | | | | |
|----|---------------------|-----|---|---|--|--|
| 4. | Tray dryer | B | Whole, Slice chunks, pastes | Improved product recovery Increased efficiency | Conduction heating mode and central air distribution results in non-uniform heating Degradation of temperature sensitive components | Intermittent drying and use of heat pump for dehumidification |
| 5. | Tunnel dryer | C | Whole Slices, chunks, | Controlled temperature and humidity of circulated air Most efficient flexible drying system widely used | Thermal efficiency of tunnel dryer is low 38-42%. High heat consumption Oxidation of food components | For improved efficiency simulation of thermal data for modelling of drying parameters. Can be use with as solar assisted tunnel dryer |
| 6. | Drum drying | C | Highly viscous Pastes, puree slurries, solutions | High drying rate Variety of product obtained Suitable for high solids and sugar rich slurries of Fruits and Vegetable | Low throughput Difficulty in scraping-off sugar rich foods Heated surface drying may result in cooked flavour, Non-enzymatic browning High heat consumption Humidification in the processing area due to evaporation | Heat transfer increment by imprinting streams Vacuum drum drying Turbo dryer (three pass drum dryer with specifically designed heat exchanger and cyclone separator) Cooling mechanism eases the scraping-off of sugar rich foods |
| 6. | Spray drying | B | Low viscous solutions, slurries | Very fine high quality powder production Very large contact surface area Suitable for high moisture foods | Difficulty in drying of sugar rich foods Dust production and stickiness problem in powders Size of the equipment required to achieve drying is very large Fatty feeds needs pre-preparation before atomization High shear action during atomization may also make this technique unsuitable for products sensitive to mechanical damage. | For sugar rich foods CFD to monitor efficiency design of spray chamber Multistage spray dryer (2-3 stages) generally with fluidized bed dryer ultrasonic atomizers, superheated steam as drying media to reduce wall deposition |
| 7. | Fluidized bed dryer | B/C | Whole, particulates granular, even slurries, pastes solutions that can be fluidized | very high heat and mass transfer extremely high contact surface area better quality of products high level intermixing of particulate phase | Thermal efficiency is about 40-80% Too much undesirable dust Restriction on particle size | Pulsed flows, Intermittent, local fluidization/spouting, Mechanical agitation, Conductive heat transfer (internal heat exchangers), jacket heating and combination drying (Heat pump, spray dryer, freeze dryer) Sticking and product accumulation in continuous dryers is largely prevented by vibrating the fluid bed |
| 8. | Freeze drying | B | Slices, pastes, slurries, solutions | Best quality product with retention of max heat sensitive components High porosity and rehydration capacity of products. | Very long drying times Uneconomical | Hybrid drying to make it economical. Pre and post drying treatment such as spray drying, osmodehydration. |

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|-----|---------------------------------|-----|---|--|--|--|
| 9. | Vacuum drying | B/C | Whole, Slices Chunks, paste, puree slurries, granules, solutions | High drying rate, and a reduction in shrivelling High shrinkage and rehydration ratio | Long drying times Product darkening due to high pressure | Used in hybrid drying with conventional and novel drying methods such as drum drying, supersteam, osmodehydrated, solar assisted Microwave, Infrared, rotary, Ohmic heating. |
| 10. | Osmotic drying | B/C | Whole, Slices Chunks, pieces | Minimizes heat effect and use of chemical treatment as preservative Retention of volatile components. Improved texture and Structurability Energy efficient | Two-step process Change in product taste Excessive waste of osmotic solution Breakage of food pieces during flow of syrup (Continuous process) and mechanical agitation (batch process) Leaching out of colour, acids, sugars, minerals, vitamins | Used as pre-treatment in various thermal and non-thermal processes as hot air drying, freeze, vacuum, tray, microwave drying etc |
| 11. | Refractance window drying | B | Puree, liquids | Similar to drum drying only low temperature heating (70-85°C) Short drying time 3-5 minutes High thermal efficiency (77- 52%), In expensive (approx. Half the cost of freeze drying) | | |

*B: Batch, **C: Continuous

2. Conclusion

Drying is an important unit operation. Drying of food products has been a very important industrial sector for many years. This is also reflected in the continuing improvement in drying technique. Continuous improvement in drying technique is triggered by handling complex foods, improving product quality reducing costs and energy efficiency of the driers. As standard of living rises the demand for energy-efficient, faster, environmentally friendly and cost-effective drying technologies will continue to increase worldwide. As the fuel prices rise, it is necessary to develop sustainable drying technologies using renewable sources using innovative ideas. Thus we can say that, drying is an ancient process which is still continuing providing food security and increasing industrialization of foods.

3. Future Scope

Drying R&D seems to have reached a sustainable level of activity around the globe; still there is tremendous scope to carry out R&D in this complex process. As energy costs, energy efficiency will be key criterion for marketing of dryers. Much R&D needs to be done to make some of the new concepts commercially attractive.

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